Rapid Communications

Convection driven by internal heat sources and sinks: Heat transport beyond the mixing-length or "ultimate" scaling regime

Benjamin Miquel[®],^{*} Simon Lepot, Vincent Bouillaut, and Basile Gallet Service de Physique de l'Etat Condensé, CEA, CNRS UMR 3680, Université Paris-Saclay, CEA Saclay, 91191 Gif-sur-Yvette, France

(Received 23 July 2019; published 19 December 2019)

Thermal convection driven by internal heat sources and sinks was recently shown experimentally to exhibit the mixing-length or "ultimate" scaling-regime: The Nusselt number Nu (dimensionless heat flux) increases as the square-root of the Rayleigh-number Ra (dimensionless internal temperature difference). While for standard Rayleigh-Bénard convection this scaling regime was proven to be a rigorous upper bound on the Nusselt number, we show that this is not so for convection driven by internal sources and sinks. To wit, we introduce an asymptotic expansion to derive steady nonlinear solutions in the limit of large Ra₀, the Rayleigh-number based on the strength of the heat source. We illustrate this procedure for a simple sinusoidal heat source and show that it achieves heat transport enhancement beyond the mixing-length scaling regime: Nu increases linearly with Ra over this branch of solutions. Using rigorous upper bound theory, we prove that the scaling regime Nu \sim Ra of the asymptotic solution corresponds to a maximization of the heat flux subject to simple dynamical constraints, up to a dimensionless prefactor. Not only do two-dimensional numerical simulations confirm the analytical solution for the sinusoidal source, but, more surprisingly, they indicate that it is stable and indeed achieved by the system up to the highest Ra_O investigated numerically, with a heat transport efficiency orders of magnitude higher than the standard mixing-length estimate.

DOI: 10.1103/PhysRevFluids.4.121501

Motivated by studies of the Rayleigh-Bénard (RB) system, a fluid layer enclosed between a hot bottom plate and a cold top one, Malkus put forward the physical idea that turbulent convection may maximize the heat transport subject to simple dynamical constraints (the "power integrals") [1]. Howard introduced the corresponding variational problem and obtained an upper bound on the heat transport enhancement achieved by RB convection [2]. Busse improved the approach by including the incompressibility constraint and deriving the so-called "multi- α " solutions to the variational problem [3]. He also showed that a similar approach can be applied to many transport problems, such as momentum transport in a turbulent shear flow [4,5]. In the 1990s, Doering and Constantin introduced an alternate method, the "background method," to derive similar bounds for a broad range of turbulent flows [6-8]. In the context of RB convection, these rigorous upper bounds show that the Nusselt number Nu (dimensionless heat flux) increases at most like the square-root of the Rayleigh number Ra (dimensionless temperature difference between the plates) in the large-Rayleigh-number regime [2,3,8]. The scaling behavior of this upper bound is reminiscent of the "mixing-length" arguments put forward in astrophysical contexts, where it is assumed that the relation between the heat flux and the temperature difference does not involve the molecular diffusivities [9,10]. The resulting "mixing-length" scaling law is Nu $\sim \sqrt{\Pr Ra}$, where Pr is the Prandtl number. In

^{*}benjamin.miquel@cea.fr

the context of RB convection, this scaling regime was initially proposed by Kraichnan [11], albeit with additional logarithmic corrections, and is sometimes referred to as the "ultimate" regime of thermal convection [12]. The actual scaling behavior Nu ~ Ra^{γ} of experimental RB convection remains a controversial issue in the literature, with values of the measured exponent γ in the range $\gamma = 0.33$ –0.39 for the highest Ra achievable in the laboratory [12–17]. This is clearly below the scaling exponent of the upper bound derived by Howard and improved upon by several authors: RB convection does not seem to maximize the heat flux constrained by the power integrals alone.

It was soon realized that the boundary layers—either laminar or turbulent—are responsible for the reduced value of the exponent γ [1,11,18]. Various approaches were designed to remove these boundary layers, with the goal of achieving the mixing-length scaling regime predicted by Spiegel for bulk convection inside astrophysical objects [9,10]. The most drastic one consists in numerically simulating "homogeneous" convection inside a 3D-periodic domain [19]. While early results of this approach point towards a Nu $\sim Ra^{1/2}$ scaling relation, further investigation indicates that the numerical simulations are polluted by diverging elevator-mode solutions at high Ra. The latter would grow unboundedly if resolution- and numerical-noise-dependent instabilities did not eventually saturate their amplitude [20,21]: At the mathematical level, the consequence is that the Nusselt number can take arbitrarily large values, making the physical relevance of this configuration questionable. One way around this issue is to consider very tall domains, a situation approached experimentally using convection cells that consist in a narrow vertical channel connecting two reservoirs of hot and cold fluid. Interestingly, the data then displays a square-root relation between the heat flux and the internal temperature gradient [22,23]. However, the associated Rayleigh and Nusselt numbers need be built using the width of the channel [24-26]. The resulting scaling relation between the heat flux and the internal temperature gradient explicitly involves the width of the domain, which challenges its applicability to the arbitrarily wide domains characteristic of astrophysical and geophysical flows. Another line of work consists in replacing the smooth boundaries of RB convection by rough plates. When the roughness has a single scale, it can lead to $\gamma \simeq 0.5$ over a finite range of Rayleigh numbers, the belief being that this range extends to arbitrarily large Ra when the roughness involves infinitely many scales in a fractal fashion [27–37].

Recently, some of the authors developed an alternate convection experiment, where heat is effectively input and extracted in volume through a combination of radiative heating and secular cooling [38,39]. This strategy allowed us to bypass the diffusive boundary layers and achieve the mixing-length scaling regime Nu ~ Ra^{1/2}. The questions that naturally arise are thus: Does convection driven by heat sources and sinks maximize heat transport, and how large is the associated maximum heat flux? We answer this question by combining two theoretical tools: First, we introduce an asymptotic expansion to derive high-Rayleigh-number steady solutions [40–42]. Second, we derive rigorous upper bounds on the heat transport efficiency of convection driven by internal sources and sinks. Because the scaling behavior of the asymptotic solution matches the one of the upper bound, we can conclude unambiguously on the maximum heat transport enhancement that can actually be achieved in the system: the asymptotic solution obeys the scaling law Nu ~ Ra, which corresponds to heat transport enhancement much beyond the mixing-length scaling regime.

Convection driven by heat sources and sinks. Consider a Newtonian fluid of mean density ρ_0 , specific heat capacity C, kinematic viscosity ν , and thermal diffusivity κ , inside a domain of height H. The fluid is subject to internal heat sources and sinks, which enter the heat equation through a term $Q_0S(z)$, where Q_0 characterizes the magnitude of the heat input/output in Watts per cubic meter, z is the vertical coordinate measured in units of H, and S(z) is a shape function that depends on the dimensionless vertical coordinate z only. This heating/cooling profile S(z) has zero mean over the fluid domain, to avoid any temperature drift in the long-time limit, and unit root-mean-square (rms) value. After nondimensionalizing lengths with H, time with H^2/κ , and temperature with

 $\nu\kappa/\alpha gH^3$, where α is the thermal expansion coefficient and g is gravity, the Navier-Stokes and heat equations in the Boussinesq approximation read:

$$\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla p + \Pr(\Delta \mathbf{u} + T \mathbf{e}_z), \tag{1}$$

$$\partial_t T + \mathbf{u} \cdot \nabla T = \Delta T + \operatorname{Ra}_O S(z). \tag{2}$$

In these equations, t and x denote the dimensionless time and space variables, while \mathbf{u} , T, and p are the dimensionless velocity, temperature, and generalized pressure fields, respectively. The velocity field is incompressible, $\nabla \cdot \mathbf{u} = 0$, and the two dimensionless control parameters appearing in the equations are the Prandtl number Pr and the flux-based Rayleigh number Ra_O, defined as

$$\Pr = \frac{\nu}{\kappa}, \quad \operatorname{Ra}_{Q} = \frac{\alpha g Q_0 H^{5}}{\rho_0 C \kappa^2 \nu}.$$
(3)

High-Rayleigh-number asymptotics. We first consider two-dimensional (2D) asymptotic solutions to Eqs. (1) and (2) where the fields depend on x and z only. For brevity, we consider a square domain $(x, z) \in \mathcal{D} = [0, 1]^2$, although the approach remains valid for an arbitrary aspect ratio. Introducing a stream function ψ such that the velocity field is $\mathbf{u} = \nabla \times (\psi \mathbf{e}_y)$, with \mathbf{e}_y the unit vector along y, Eqs. (1) and (2) yield

$$\partial_t \Delta \psi + J(\psi, \Delta \psi) = \Pr\left[\Delta^2 \psi + \partial_x T\right],$$
(4a)

$$\partial_t T + J(\psi, T) = \Delta T + \operatorname{Ra}_Q S(z),$$
(4b)

where the Jacobian is $J(A, B) = \partial_x A \partial_z B - \partial_z A \partial_x B$. For simplicity, we consider stress-free boundary conditions at all boundaries of the square domain: $\psi = 0$, $\Delta \psi = 0$. We consider insulating boundary conditions at the vertical sidewalls ($\partial_x T = 0$), and we leave the top and bottom thermal boundary conditions unspecified for now.

We seek a time-independent asymptotic solution at high Ra_Q and thus expand the fields in powers of $Ra_Q^{1/2}$:

$$\psi = \operatorname{Ra}_{Q}^{1/2}\psi_{0} + \psi_{1} + \operatorname{Ra}_{Q}^{-1/2}\psi_{2} + \dots,$$
(5)

$$T = \operatorname{Ra}_{Q}^{1/2} T_{0} + T_{1} + \operatorname{Ra}_{Q}^{-1/2} T_{2} + \dots$$
(6)

At order $\mathcal{O}(Ra_Q)$, Eqs. (4) yield, respectively,

$$J(\psi_0, \Delta \psi_0) = 0, \tag{7a}$$

$$J(\psi_0, T_0) = S(z).$$
 (7b)

To lowest order, the flow thus satisfies the Euler equation and advects heat from the sources to the sinks, without the need for diffusive processes. The solution to Eq. (7a) is simply

$$\Delta \psi_0 = F(\psi_0),\tag{8}$$

i.e., the vorticity is a function of the stream function, with the only constraint that F(0) = 0 to satisfy the stress-free boundary conditions. The solutions are very degenerate at this stage: F can be chosen arbitrarily, the corresponding temperature field being then deduced from Eq. (7b). As we will now see, solvability conditions at the next order constrain the choice of F. Equation (4a) yields at order $\mathcal{O}(\text{Rao}^{1/2})$:

$$J(\psi_0, \Delta \psi_1) + J[\psi_1, F(\psi_0)] = \Pr(\partial_x T_0 + \Delta^2 \psi_0),$$
(9)

where we have inserted the relation Eq. (8). Multiplying this equation by $G(\psi_0)$, with G an arbitrary differentiable function, before integrating over the square domain \mathcal{D} , leads to

$$\iint_{\mathcal{D}} G(\psi_0) \{ J(\psi_0, \Delta\psi_1) + J[\psi_1, F(\psi_0)] \} dx dz = \Pr \iint_{\mathcal{D}} G(\psi_0) (\partial_x T_0 + \Delta^2 \psi_0) dx dz.$$
(10)

For any three functions *a*, *b*, and *c*, one of which vanishes at the boundaries of \mathcal{D} , the functions can be swapped inside triple products of the form $\iint_{\mathcal{D}} aJ(b, c) dxdz$ at the expense of changing the sign. Using this property, one can prove that the left-hand side of Eq. (10) vanishes, giving the following constraints on ψ_0 and T_0 :

$$\iint_{\mathcal{D}} G(\psi_0)(\partial_x T_0 + \Delta^2 \psi_0) dx dz = 0, \tag{11}$$

for any differentiable function G.

To summarize, solving this problem consists in finding the function F in Eq. (8), such that ψ_0 satisfies the infinite set of solvability conditions Eq. (11), where the temperature field T_0 is deduced from ψ_0 by solving Eq. (7b). This is an intricate task in general, that may not even always admit a solution. In the following, we thus focus on a simple form for the source function S(z) to provide an explicit example of solution to this problem.

Sinusoidal heating. The procedure described above becomes surprisingly simple in the situation where the source term varies sinusoidally in the vertical direction, with a shape function $S(z) = \sqrt{2} \sin(2\pi z)$. One can look for solutions to Eqs. (7) that consist of the gravest Fourier mode only:

$$\psi_0 = \psi_m \sin(\pi x) \sin(\pi z), \tag{12a}$$

$$T_0 = T_m \cos(\pi x) \sin(\pi z). \tag{12b}$$

Substitution into Eq. (7b) yields $T_m = 2\sqrt{2}/\pi^2 \psi_m$. At this stage, the amplitude ψ_m remains undetermined, and we have obtained a continuous family of solutions to the undamped equations. The selection of ψ_m occurs through the solvability conditions Eq. (11), which are simultaneously ensured if $\partial_x T_0 + \Delta^2 \psi_0 = 0$. After substitution of Eqs. (12a) and (12b), this yields $\psi_m = \pm 2^{-1/4} \pi^{-5/2}$ and $T_m = \pm 2^{7/4} \pi^{1/2}$. This completes the determination of the asymptotic solution.

To check the validity of this solution, we performed direct numerical simulations (DNS) of the governing Eqs. (4a) and (4b) with the pseudospectral solver CORAL [43]. We time-stepped the equations inside the domain $[x, z] \in [0, 1]^2$ with stress-free boundaries and insulating sidewalls. We consider either vanishing-temperature or insulating boundary conditions at top and bottom. In the latter case, we set the spatially averaged temperature to zero initially, and it remains zero under the evolution Eq. (4b). Remarkably enough, the system settles in a steady solution in the long-time limit. In Fig. 1, we show the temperature field of these steady states for various Ra_{Ω} . The analytical solution derived above readily satisfies T = 0 at top and bottom, and the numerical solutions indeed tend to the theoretically predicted shape as Ra_O becomes larger and larger. For no-flux boundary conditions, small boundary layers develop at the top and bottom to match the analytical solution-valid in the bulk-to the no-flux boundary conditions. Methods to compute such boundary-layer corrections in a square box are provided in Refs. [40,44,45]. In the present situation, these boundary layers have a negligible impact on the temperature field for large Ra_O, and the solution again takes the shape of the asymptotic analytical prediction; see Fig. 1. For a more quantitative comparison, we plot in Fig. 2 the spatial maximum of ψ and T in steady state, as functions of Ra_Q. At large Ra_Q, they are in excellent agreement with the predictions Ra_Q^{1/2} $|\psi_m|$ and $\operatorname{Ra}_{O}^{1/2}|T_{m}|$ of the asymptotic approach.

Beyond the ultimate regime. To facilitate the comparison to other convective systems, we now express the asymptotic results in terms of standard Rayleigh and Nusselt numbers. We introduce the Rayleigh number Ra based on the rms temperature, a good proxy for the typical temperature difference inside the square domain. In terms of the dimensionless temperature field, this Rayleigh number is simply $Ra = \sqrt{\langle T^2 \rangle}$, where $\langle \cdot \rangle$ denotes space and time average. The Nusselt number is then defined as $Nu = Ra_Q/Ra$. Up to a dimensionless prefactor depending on the source function S(z), this number is the ratio of the heat flux transferred from the heat sources to the sinks, to the hypothetical heat flux associated with pure diffusion of the rms temperature over the domain height. Equivalently, Nu is proportional to the ratio of the rms temperature of the diffusive steady solution to the rms temperature of the convective one.

CONVECTION DRIVEN BY INTERNAL HEAT SOURCES ...



FIG. 1. Temperature field in steady state obtained by DNS of Eqs. (4a) and (4b), for no-flux [top row (a-e)] and vanishing-temperature [bottom row (f-j)] boundary conditions at top and bottom. The Prandtl number is Pr = 1 and the flux-based Rayleigh number Ra_Q increases from left to right. All fields are normalized by the spatial maximum max[T(x, z)]. We represent isocontours for equispaced values indicated in panel (c).

Taking the rms value of Eq. (12b), remembering that $T = \text{Ra}_{Q}^{1/2}T_{0}$ to lowest order, we obtain $\text{Ra} = \text{Ra}_{Q}^{1/2} |T_{m}|/2$. Substituting the expression of T_{m} and $\text{Ra}_{Q} = \text{Nu} \times \text{Ra}$ leads to

$$Nu = \frac{Ra}{2^{3/2}\pi}.$$
 (13)

The asymptotic solution corresponds to heat transport enhancement beyond the mixing-length or "ultimate" scaling regime Nu $\sim \sqrt{\text{Ra Pr}}$. This new scaling-regime can be traced back to the laminar



FIG. 2. Spatial maximum of the stream function and temperature field as functions of the flux-based Rayleigh number. Symbols correspond to the steady state attained at large time in the DNS with insulating (orange; light gray) or vanishing-temperature (blue; dark gray) top and bottom boundary conditions. The dashed and dash-dotted lines are the predictions $Ra_Q^{1/2}|\psi_m|$ and $Ra_Q^{1/2}|T_m|$ from the asymptotic theory.

nature of the flow: The typical velocity is set by the balance between the buoyancy force and the viscous term of the Navier-Stokes equation, which yields a Reynolds number $\text{Re} \sim \text{Ra/Pr}$, as opposed to the standard free-fall estimate $\text{Re} \sim (\text{Ra/Pr})^{1/2}$ associated with the mixing-length regime of thermal convection [9,10]. This fast flow efficiently carries fluid elements from the heat sources to the sinks, leaving them little time to build large temperature values.

Bound on the heat transport. The scaling law Eq. (13) may come as a surprise to readers familiar with Rayleigh-Bénard convection. Indeed, as mentioned at the outset, for the latter setup one can prove rigorous upper bounds on the Nusselt number of the form Nu $\leq C \operatorname{Ra}^{1/2}$ [2,8], where C is a dimensionless constant, incompatible with scaling laws of the form (13). This apparent paradox is solved by observing that these upper bounds only hold for Rayleigh-Bénard-like geometries, and not for convection driven solely by internal sources and sinks. One may thus wonder how large the Nusselt number can be for convection driven by heat sources and sinks. We answer this question by deriving a rigorous upper bound on the Nusselt number for this situation. We consider the general three-dimensional situation, Eqs. (1) and (2), inside a parallelepipedic domain of arbitrary aspect ratio, with insulating and either stress-free or no-slip boundary conditions at each boundary. Once again, without loss of generality we set the spatially averaged temperature to zero initially, and it remains zero at any subsequent time. Multiplying Eq. (2) by S(z) before taking a space and time average yields, after a few integrations by parts:

$$\operatorname{Ra}_{Q} = -\langle S'(z)wT \rangle - \langle S''(z)T \rangle + [S'(z)\overline{T}(z)]_{0}^{1},$$
(14)

where $\overline{T}(z)$ denotes the horizontally- and time-averaged temperature profile, and primes denote *z*-derivatives of the source. We introduce the numerical constants $c_1 = \max_{z \in [0;1]} |S'(z)|$ and $c_2 = \sqrt{\langle S''(z)^2 \rangle}$ and apply the Cauchy-Schwarz inequality to Eq. (14) to obtain

$$\operatorname{Ra}_{Q} \leqslant c_{1}(\sqrt{\langle w^{2} \rangle}\operatorname{Ra} + |\overline{T}(0)| + |\overline{T}(1)|) + c_{2}\operatorname{Ra}.$$
(15)

In a similar fashion, multiplying Eq. (2) by T before averaging yields

$$\langle |\nabla T|^2 \rangle = \operatorname{Ra}_Q \langle S(z)T \rangle \leqslant \operatorname{Ra}_Q \operatorname{Ra},$$
 (16)

where we have used $\langle S(z)^2 \rangle = 1$ and $\sqrt{\langle T^2 \rangle} = \text{Ra.}$

Because
$$\langle T \rangle = 0$$
, there is a $z_0 \in [0; 1]$ such that $\overline{T}(z_0) = 0$. Hence, $|\overline{T}(1)| = |\int_{z_0}^1 \partial_z \overline{T} dz| \leq \sqrt{\int_{z_0}^1 (\partial_z \overline{T})^2 dz} \leq \sqrt{\langle |\nabla T|^2 \rangle} \leq \sqrt{\operatorname{Ra}_Q \operatorname{Ra}}$, and similarly $|\overline{T}(0)| \leq \sqrt{\operatorname{Ra}_Q \operatorname{Ra}}$, so that

$$\operatorname{Ra}_{Q} \leqslant c_{1}(\sqrt{\langle w^{2} \rangle}\operatorname{Ra} + 2\sqrt{\operatorname{Ra}_{Q}\operatorname{Ra}}) + c_{2}\operatorname{Ra}.$$
(17)

Dotting the Navier-Stokes Eq. (1) with **u** before averaging leads to the balance between dissipation and injection of kinetic energy: $\langle |\nabla \mathbf{u}|^2 \rangle = \langle wT \rangle \leq \sqrt{\langle w^2 \rangle} \text{Ra}$. We insert this inequality into the Poincaré inequality for w, which vanishes at the top and bottom boundaries:

$$\langle w^2 \rangle \leqslant \frac{\langle |\partial_z w|^2 \rangle}{\pi^2} \leqslant \frac{\langle |\nabla \mathbf{u}|^2 \rangle}{\pi^2} \leqslant \frac{\sqrt{\langle w^2 \rangle} \mathrm{Ra}}{\pi^2}.$$
 (18)

Dividing by $\sqrt{\langle w^2 \rangle}$ we obtain $\sqrt{\langle w^2 \rangle} \leq \text{Ra}/\pi^2$. Inserting the latter inequality into Eq. (17) and substituting $\text{Ra}_{\text{Q}} = \text{Nu} \times \text{Ra}$ finally leads to $\text{Nu} - c_1(2\sqrt{\text{Nu}} + \text{Ra}/\pi^2) - c_2 \leq 0$, which is satisfied only if

Nu
$$\leq c_1^2 \left(1 + \sqrt{1 + \frac{c_2}{c_1^2} + \frac{\mathbf{Ra}}{c_1 \pi^2}} \right)^2.$$
 (19)

This inequality is the desired upper bound on the Nusselt number. The right-hand side scales linearly in Ra for large Rayleigh number, which shows that the Nusselt number cannot increase faster than linearly in Ra in the present system. For the particular case of sinusoidal heating, the



FIG. 3. Dimensionless heat flux Nu = Ra_Q/Ra as a function of Ra = $\sqrt{\langle T^2 \rangle}$. Same color code as in Fig. 2. Dashed line: asymptotic solution [Eq. (13)]. Dash-dotted line: analytic upper bound [Eq. (19)].

constants entering expression Eq. (19) are $c_1 = 2\sqrt{2\pi}$ and $c_2 = 4\pi^2$. The upper bound becomes Nu $\leq 2\sqrt{2} \operatorname{Ra}/\pi$ at leading order in Ra $\gg 1$. The heat flux Nu = Ra/ $2\sqrt{2\pi}$ of the asymptotic solution Eqs. (12a) and (12b) thus saturates the analytical bound up to a dimensionless prefactor equal to 8 (see Fig. 3), and the bound can only be marginally improved upon. One may want to express the bound Eq. (19) using Rayleigh and Nusselt numbers even more closely related to the standard definitions of RB convection. For instance, we introduce a Rayleigh number based on a characteristic maximum temperature Ra_{max} = max₂[$\overline{T^2}(z)$]^{1/2}, where the overbar still denotes a horizontal and time average, together with the associated Nusselt number Nu_{max} = Ra_Q/Ra_{max}. An application of Hölder's inequality leads to Ra $\leq \operatorname{Ra}_{max}$ and Nu_{max} \leq Nu, so that Eq. (19) holds when Ra and Nu are replaced by Ra_{max} and Nu_{max}.

Discussion. We have derived upper bounds on the Nusselt number, as well as steady asymptotic solutions, that exhibit a heat transport scaling law Nu \sim Ra, beyond the mixing-length or "ultimate" scaling regime. A natural next step would be to study the stability of such solutions. For the sinusoidal heat source in 2D, the energy of the convective flow concentrates in the gravest Fourier modes. This observation suggests-and one may be able to prove analytically-that the asymptotic solution is indeed stable at arbitrarily large Ra_O, in a similar fashion to 2D flows forced at the largest scale [46]. In our numerical computations we reached $Ra_0 \approx 10^{11}$ and $Re \approx 4.10^4$ without observing signs that the large-scale steady solution would become unstable. However, for more general source functions and in the general 3D situation with no-slip boundary conditions, we observe unsteady and turbulent flows in both experiments and DNS, with an average heat flux obeying the mixing-length scaling law [38,39]. Steady solutions of the form of Eqs. (7b), (8), and (11) remain useful in this context, because they show that the upper bound Eq. (19) is sharp, i.e., it captures the scaling behavior of some true solutions to the equations. Improving the scaling behavior of such bounds would thus require a technology to exclude some unstable solutions during the bounding procedure, a formidable task in general [47]. Instead, we speculate that the combination of the asymptotic solutions described above with the upper bound Eq. (19) could be indicative of the scaling behavior of extreme events of heat transport: Keeping in mind the picture of a chaotic system that wanders between unstable solutions and periodic orbits in phase space [48–50], unstable solutions of the form of Eqs. (7b), (8), and (11) may set the scaling behavior for such extreme events, with Nu \sim Ra over the duration of a single event.

Acknowledgments. We thank C. R. Doering, G. Fantuzzi, and D. Goluskin for insightful discussions. This work is supported by the European Research Council under Grant Agreement No. 757239 and by Agence Nationale de la Recherche under Grant No. ANR-10-LABX-0039.

- W. V. R. Malkus, The heat transport and spectrum of thermal turbulence, Proc. Roy. Soc. A 225, 196 (1954).
- [2] L. N. Howard, Heat transport by turbulent convection, J. Fluid Mech. 17, 405 (1963).
- [3] F. H. Busse, On Howard's upper bound for heat transport by turbulent convection, J. Fluid Mech. 37, 457 (1969).
- [4] F. H. Busse, Bounds on the transport of mass and momentum by turbulent flow between parallel plates, Z. Angew. Math. Phys. 20, 1 (1969).
- [5] F. H. Busse, Bounds for turbulent shear flow, J. Fluid Mech. 41, 219 (1970).
- [6] C. R. Doering and P. Constantin, Energy Dissipation in Shear Driven Turbulence, Phys. Rev. Lett. 69, 1648 (1992).
- [7] C. R. Doering and P. Constantin, Variational bounds on energy dissipation in incompressible flows: Shear flow, Phys. Rev. E 49, 4087 (1994).
- [8] C. R. Doering and P. Constantin, Variational bounds on energy dissipation in incompressible flows. III. Convection, Phys. Rev. E 53, 5957 (1996).
- [9] E. A. Spiegel, A generalization of the mixing-length theory of thermal convection, ApJ 138, 216 (1963).
- [10] E. A. Spiegel, Convection in stars I. Basic Boussinesq convection, Annu. Rev. Astron. Astrophys. 9, 323 (1971).
- [11] R. H. Kraichnan, Turbulent thermal convection at arbitrary Prandtl number, Phys. Fluids 5, 1374 (1962).
- [12] X. Chavanne, F. Chillà, B. Castaing, B. Hébral, B. Chabaud, and J. Chaussy, Observation of the Ultimate Regime in Rayleigh-Bénard Convection, Phys. Rev. Lett. 79, 3648 (1997).
- [13] J. J. Niemela, L. Skrbek, K. R. Sreenivasan, and R. J. Donnelly, Turbulent convection at very high Rayleigh numbers, Nature 404, 837 (2000).
- [14] X. Chavanne, F. Chillà, B. Chabaud, B. Castaing, and B. Hébral, Turbulent Rayleigh-Bénard convection in gaseous and liquid He, Phys. Fluids 13, 1300 (2001).
- [15] G. Ahlers, S. Grossmann, and D. Lohse, Heat transfer and large-scale dynamics in turbulent Rayleigh-Bénard convection, Rev. Mod. Phys. 81, 503 (2009).
- [16] P.-E. Roche, F. Gauthier, R. Kaiser, and J. Salort, On the triggering of the ultimate regime of convection, New J. Phys. 12, 085014 (2010).
- [17] X. He, D. Funfschilling, H. Nobach, E. Bodenschatz, and G. Ahlers, Transition to the Ultimate State of Turbulent Rayleigh-Bénard Convection, Phys. Rev. Lett. 108, 024502 (2012).
- [18] S. Grossmann and D. Lohse, Scaling in thermal convection: A unifying theory, J. Fluid Mech. 407, 27 (2000).
- [19] D. Lohse and F. Toschi, Ultimate State of Thermal Convection, Phys. Rev. Lett. 90, 034502 (2003).
- [20] E. Calzavarini, C. R. Doering, J. D. Gibbon, D. Lohse, A. Tanabe, and F. Toschi, Ultimate state of thermal convection, Phys. Rev. E 73, 035301(R) (2006).
- [21] C. R. Doering, Thermal forcing and "classical" and "ultimate" regimes of Rayleigh-Bénard convection, J. Fluid Mech. 868, 1 (2019).
- [22] M. Gibert, H. Pabiou, F. Chillà, and B. Castaing, High-Rayleigh-Number Convection in a Vertical Channel, Phys. Rev. Lett. 96, 084501 (2006).
- [23] J.-C. Tisserand, M. Creyssels, M. Gibert, B. Castaing, and F. Chillà, Convection in a vertical channel, New J. Phys. 12, 075024 (2010).
- [24] M. L. Cholemari and J. H. Arakeri, Axially homogeneous, zero mean flow buoyancy-driven turbulence in a vertical pipe, J. Fluid Mech. 621, 69 (2009).
- [25] S. S. Pawar and J. H. Arakeri, Two regimes of flux scaling in axially homogeneous turbulent convection in vertical tube, Phys. Rev. Fluids 1, 042401(R) (2016).

- [26] B. Castaing, E. Rusaouën, J. Salort, and F. Chillà, Turbulent heat transport regimes in a channel, Phys. Rev. Fluids 2, 062801(R) (2017).
- [27] Y. Shen, P. Tong, and K.-Q. Xia, Turbulent Convection Over Rough Surfaces, Phys. Rev. Lett. 76, 908 (1996).
- [28] S. Ciliberto and C. Laroche, Random Roughness of Boundary Increases the Turbulent Convection Scaling Exponent, Phys. Rev. Lett. 82, 3998 (1999).
- [29] J.-C. Tisserand, M. Creyssels, Y. Gasteuil, H. Pabiou, M. Gibert, B. Castaing, and F. Chillà, Comparison between rough and smooth plates within the same Rayleigh-Bénard cell, Phys. Fluids 23, 015105 (2011).
- [30] P. Wei, T.-S. Chan, R. Ni, X.-Z. Zhao, and K.-Q. Xia, Heat transport properties of plates with smooth and rough surfaces in turbulent thermal convection, J. Fluid Mech. 740, 28 (2014).
- [31] J. Salort, O. Liot, E. Rusaouën, F. Seychelles, J.-C. Tisserand, M. Creyssels, B. Castaing, and F. Chillà, Thermal boundary layer near roughnesses in turbulent Rayleigh-Bénard convection: Flow structure and multistability, Phys. Fluids. 26, 015112 (2014).
- [32] D. Goluskin, and C. R. Doering, Bounds for convection between rough boundaries, J. Fluid Mech. 804, 370 (2016).
- [33] Y.-C. Xie and K.-Q. Xia, Turbulent convection over rough plates with varying roughness geometries, J. Fluid Mech. 825, 573 (2017).
- [34] S. Toppaladoddi, S. Succi, and J. S. Wettlaufer, Roughness as a Route to the Ultimate Regime of Thermal Convection, Phys. Rev. Lett. 118, 074503 (2017).
- [35] X. Zhu, S. J. A. M. Stevens, R. Verzicco, and D. Lohse, Roughness-Facilitated Local 1/2 Scaling Does not Imply the Onset of the Ultimate Regime of Thermal Convection, Phys. Rev. Lett. 119, 154501 (2017).
- [36] E. Rusaouën, O. Liot, B. Castaing, J. Salort, and F. Chillà, Thermal transfer in Rayleigh-Bénard cell with smooth or rough boundaries, J. Fluid Mech. 837, 443 (2018).
- [37] X. Zhu, R. J. A. M. Stevens, O. Shishkina, R. Verzicco, and D. Lohse, Nu ~ Ra^{1/2} scaling enabled by multiscale wall roughness in Rayleigh-Bénard turbulence, J. Fluid Mech. 869, R4 (2019).
- [38] S. Lepot, S. Aumaître, and B. Gallet, Radiative heating achieves the ultimate regime of thermal convection, Proc. Natl. Acad. Sci. USA 115, 8937 (2018).
- [39] V. Bouillaut, S. Lepot, S. Aumaître, and B. Gallet, Transition to the ultimate regime in a radiatively driven convection experiment, J. Fluid Mech. 861, R5 (2019).
- [40] G. P. Chini and S. M. Cox, Large Rayleigh number thermal convection: Heat flux predictions and strongly nonlinear solutions, Phys. Fluids 21, 083603 (2009).
- [41] J. Jimenez and J. A. Zufiria, A boundary-layer analysis of Rayleigh-Bénard convection at large Rayleigh number, J. Fluid Mech. 178, 53 (1987).
- [42] F. Waleffe, A. Boonkasame, and L. M. Smith, Heat transport by coherent Rayleigh-Bénard convection, Phys. Fluids 27, 051702 (2015).
- [43] https://bitbucket.org/benmql/coral/.
- [44] S. Childress, Alpha effect in flux ropes and sheets, Phys. Earth Planet. Inter. 20, 172 (1979).
- [45] B. Gallet and W. R. Young, A two-dimensional vortex condensate at high Reynolds number, J. Fluid Mech. 715, 359 (2013).
- [46] C. Marchioro, An example of absence of turbulence for any Reynolds number, Commun. Math. Phys. 105, 99 (1986).
- [47] G. Fantuzzi, D. Goluskin, D. Huang, and S. I. Chernyshenko, Bounds for deterministic and stochastic dynamical systems using sum-of-squares optimization, SIAM J. Applied Dynamical Systems 15, 1962 (2016).
- [48] F. Waleffe, Exact coherent structures in channel flow, J. Fluid Mech. 435, 93 (2001).
- [49] G. Kawahara and S. Kida, Periodic motion embedded in plane Couette turbulence: Regeneration cycle and burst, J. Fluid Mech. 449, 291 (2001).
- [50] H. Wedin and R. Kerswell, Exact coherent structures in pipe flow: Traveling wave solutions, J. Fluid Mech. 508, 333 (2004).